

Introduction

The cost of catalyst in polymer electrolyte membrane fuel cell (PEMFC) is being reduced by increasing the activity and reducing the loading from 0.4 mgPt/cm^2 to below 0.1 mgPt/cm^2 . This results in nominal operational mass transport losses at the diffusion media/catalyst layer interface¹. Mass transport of dilute O_2 at the interface between cathode catalyst layer (CCL) and gas diffusion layer (GDL).

At -20°C , O_2 concentration dependent voltages and hydration dependent ionic conductivity will be assessed. In this work, the interfacial losses at the interface of the ultrathin film catalyst layers will be investigated. We wish to establish the relationship between different carrier gasses and diffusivity of O_2 at the gas diffusion layer. This work is on understanding ice formation mechanism in PEMFC at sub-zero temperature.

Fixture and Experimental

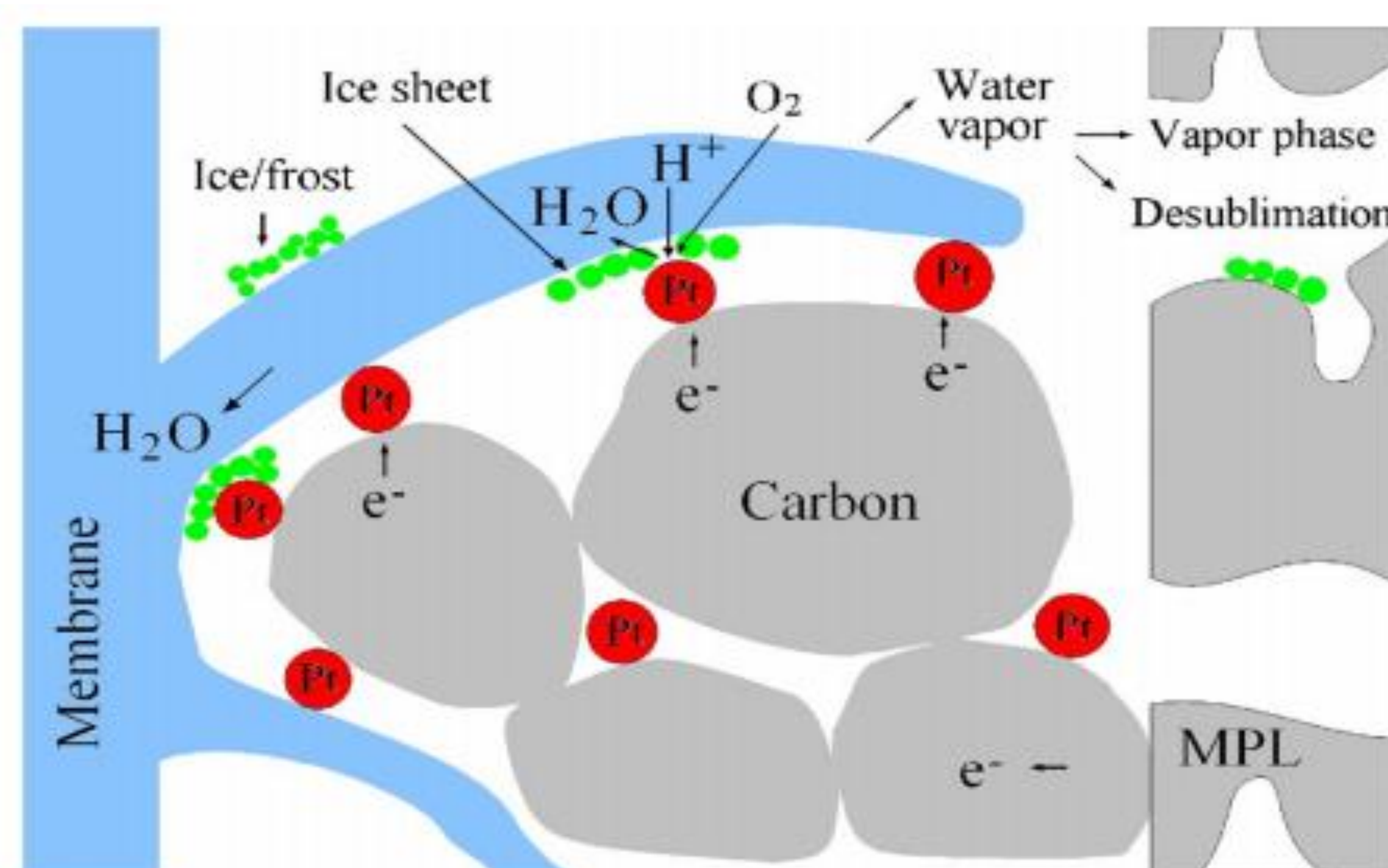
Fuel Cell Fixture

1. 16cm^2 triple pass serpentine flow fields (3/16" thick).
2. Catalyst: 0.3mgPt/cm^2 , 1.2ionomer-carbon ratio, Nafion 212 membrane. Ion Power SGL25BC.

Isothermal Water Fill Test

- Operate the cell at $T_{\text{cell}} = 80^\circ\text{C}$, 42% relative humidity (%RH) for 10 polarization curves.
- %RH condition to 75% with inert gas at $T_{\text{cell}} = 80^\circ\text{C}$.
- Freeze cell to -20°C .
- Cold start: $T_{\text{cell}} = -20^\circ\text{C}$, $I = 10\text{mA/cm}^2$. Flowrate = 0.05lpm O_2 and 0.1lpm at the anode (H_2) and cathode (O_2) respectively.

Schematic of ice formation and microscale distribution in the cathode catalyst layer.²



Freeze pre-conditioning

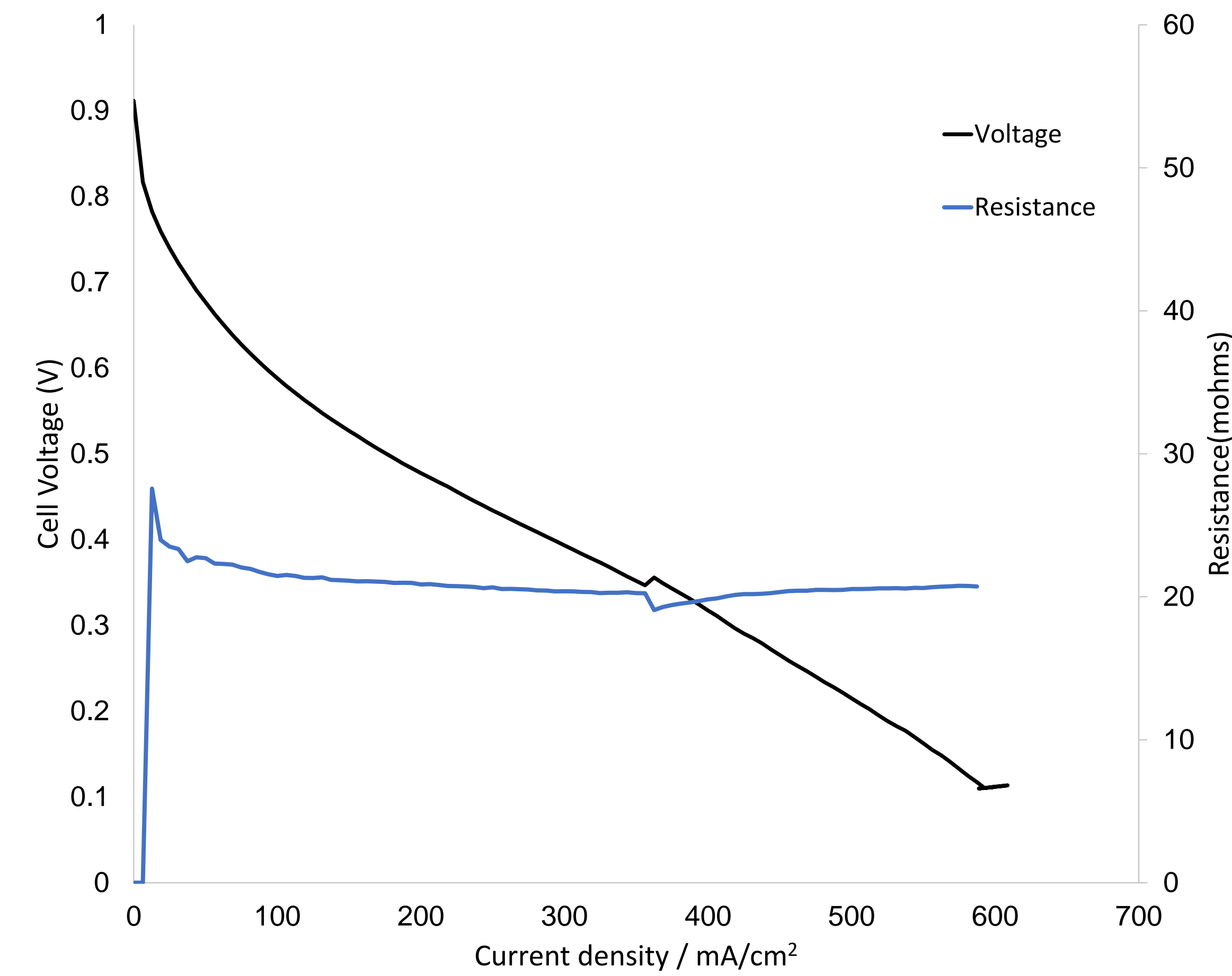


Fig 1 : Polarization at $T_{\text{cell}} = 80^\circ\text{C}$, 42% RH, stoichiometry = 2

- Preconditioning cell to stable performance by polarization.
- Resistance is low indicating good cell performance.
- Minimal mass transport losses.
- Activation losses impacts the performance of fuel cell.

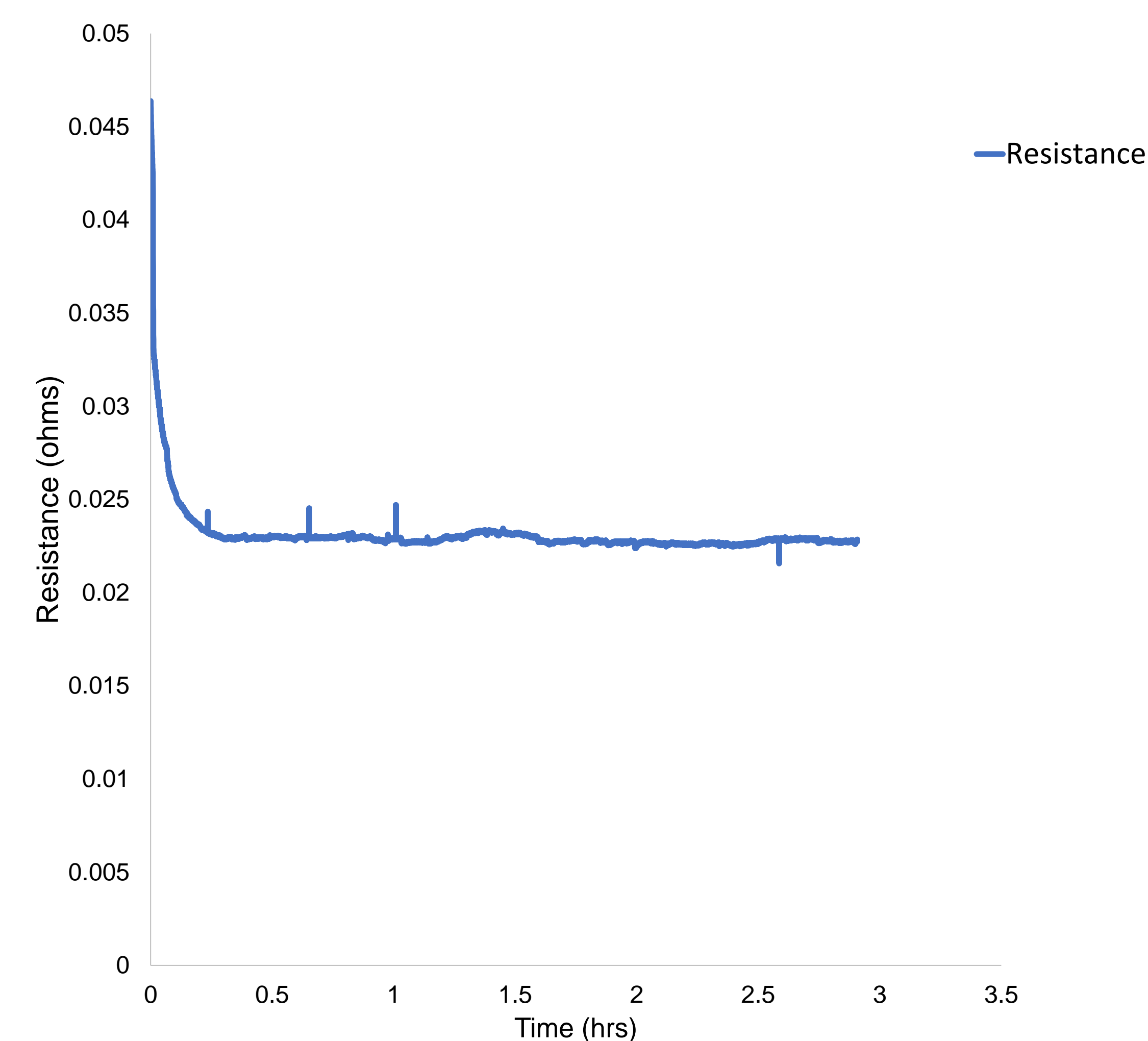


Fig 2 : Cell equilibrium conditioning $T_{\text{cell}} = 80^\circ\text{C}$, 73% RH.

- Water removed from GDL and flow channels.
- Water removed from open pores in the agglomerates
- MEA initial water content conditioned to 6 (ionomeric).
- Anode and cathode ionomer water content at equilibrium.

Isothermal Water Fill Test at -20°C

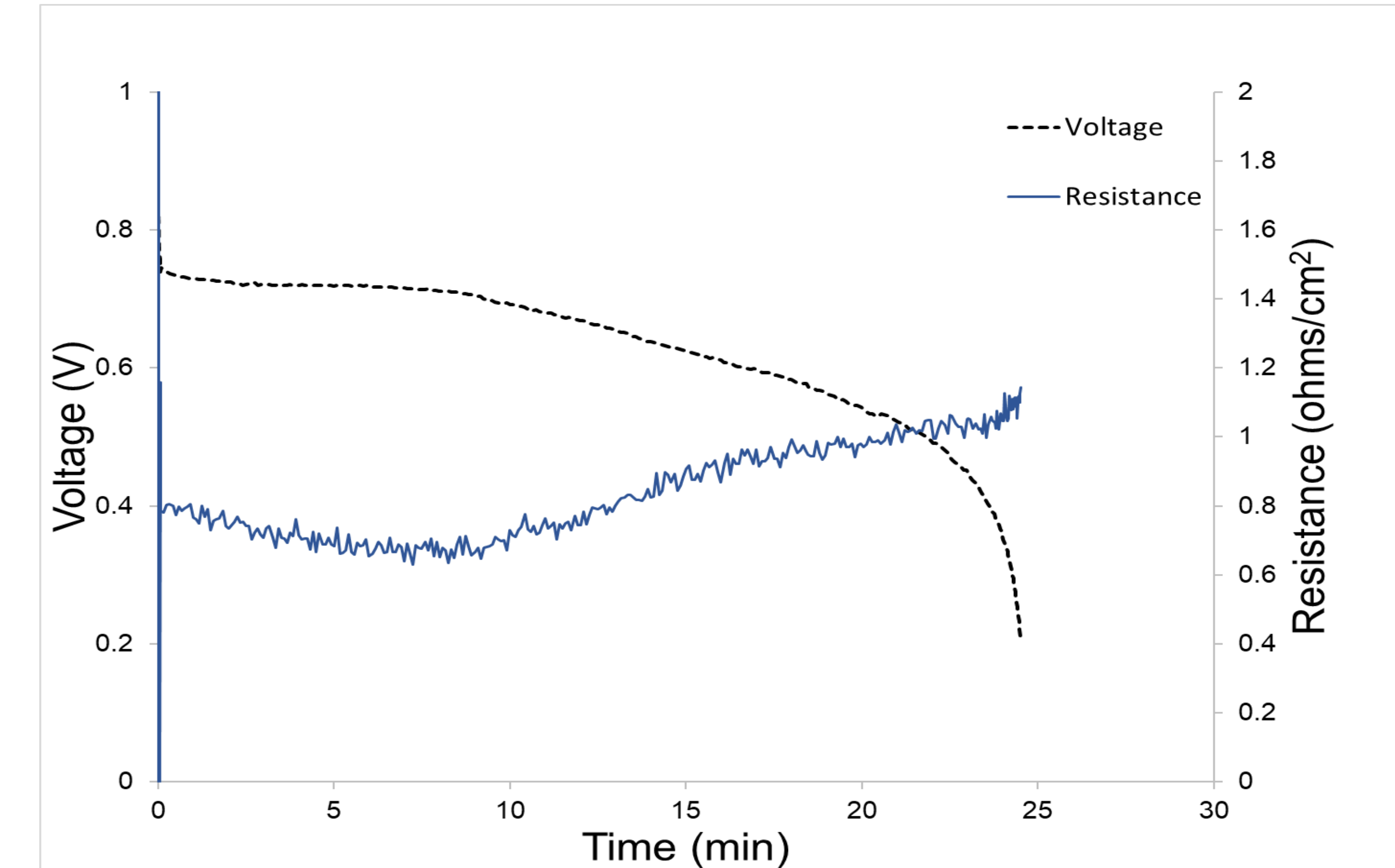


Fig 3 : Isothermal cold start at 10mA/cm^2 at $T_{\text{cell}} = -20^\circ\text{C}$.

- Membrane rehydration absent due to saturation of ionomers before cold start.
- Cell shut down due to ice accumulation in open pores.
- High mass transport resistance results from ice accumulation in open pores.
- Extended time onload due to water redistribution at low current density³.

Conclusion and Future Work

Conclusion:

- %RH removes water from the pores, GDL and flow channels allowing only water in the ionomers of the MEA.
- Ice accumulation leads to mass transport resistance which ultimately shuts down the cell at subzero temperature.

Future Work:

- Cyclic voltammogram for active area measurements.
- Electrochemical impedance spectroscopy to quantify the resistance at the thin film interface between the CL and GDL.
- Fuel Cell testing with different diluents and different oxidant concentration.

References

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2. S. Ge and C.Y. Wang *J. Electrochem. Soc.*, 154 (2) B1399 - B1406 (2007)
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