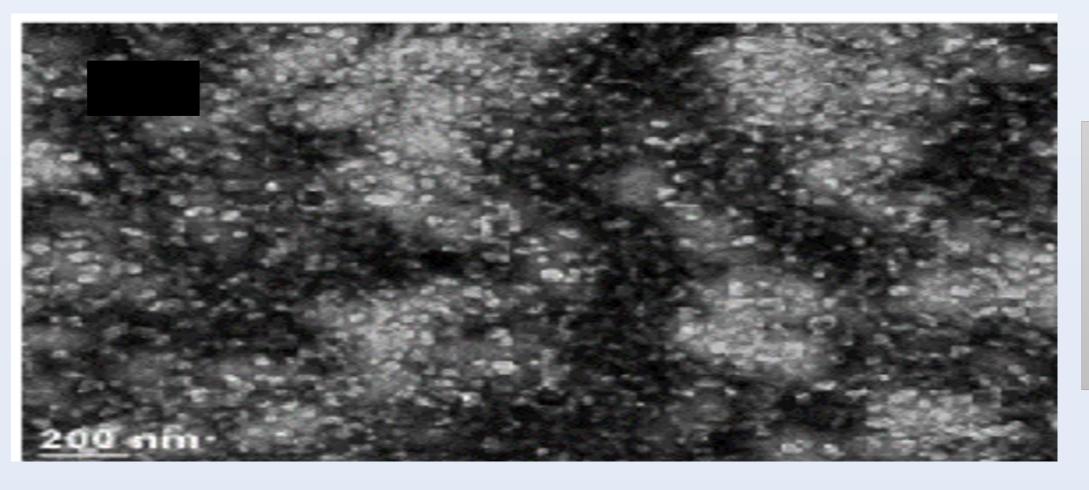


Background and Motivation

- Over the past 20 years, there has been growing interest in the formation of droplets using microfluidic approaches for
- size and the
- polydispersity index (of the droplet). These techniques have several applications summarized in fig 1 –
- Advantages of microfluidic channels include –
- considerably more control of the size and
- can be used to produce more uniform particles.
- NPs used as drug nanomedicine offer –
- Enhanced permeability
- Higher retention in vivo.
- Using a massively arrayed fiber reactor (FR), nanoparticles (NP) of PNIPAm used as drug delivery agents have been produced (see Fig 2). (Jaminkhindar et al (2006)).



Size and surface characteristics of NPs can be tuned using various process parameters, such as

- Relative flowrates of multiphases.
- Concentration of surfactant

Studies show that droplet size have a correlation with relative flow rate as modeled by the scaling Qd, Qc = flow rate of dispersed, continuous phase respectivelylaw -

Furthermore, more studies on droplet breakout in the microchannel is reveal that 3 regimes are possible at the T-junction depending on the capillary number Ca_c of the continuous fluid.

These regimes are:

- Squeezing regime ($Ca_c < 002$)
- Squeezing regime ($Ca_c < 0.002$)
- Transient regime $(0.002 < Ca_c < 0.01)$ iii)

These regimes occur due to the interplay between three forces – 1. Shear force of continuous phase on emerging droplet

2. Laplace force inside droplet dur to interfacial tension. (Thorsen et al (2001)). 3. Increase of upstream pressure in continuous phase due to droplet obstructing channel width.

w = channel width,L = channel lenght, α = characteristic constant for geometry of device,

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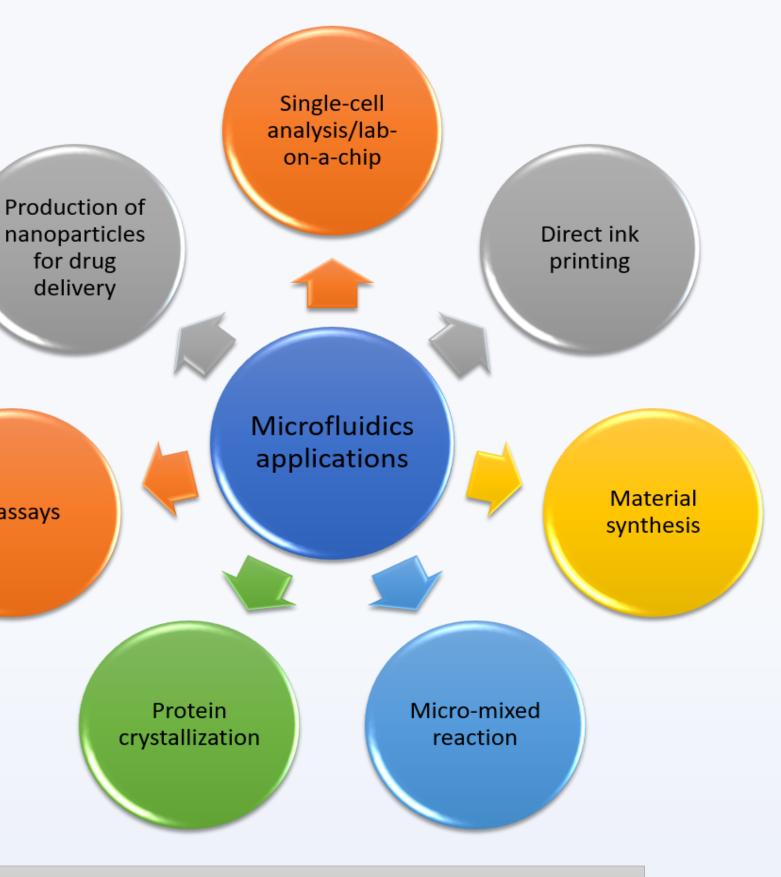


Figure 1: (above) Applications of microfluidics

Figure 2: (left)

Bioassays

TEM images of PNIPAm nanoparticles produced in the reactor. The average droplet size of 37.5nm and a PDI range of 0.26 - 0.3.

$$\frac{L}{w} = 1 + \alpha \frac{Q_d}{Q_c};$$

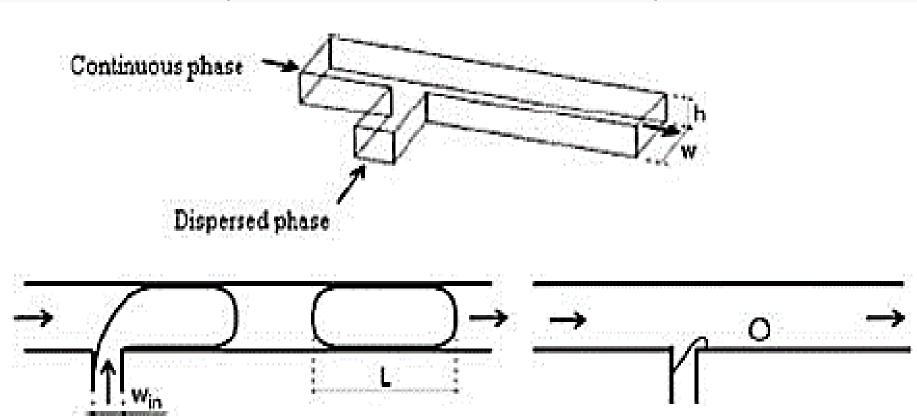
$Ca_c = \frac{U_c \mu_c}{\gamma};$

 $Uc, \mu c = flow rate, viscosity of continuous phase respectivly,$ $\gamma = interfacial tension$

About the reactor

The FR consists: massively arrayed reactor T-junction type.

• Steel fibers (diameter of 22microns)



Flow Visualization

In the study, we would like to visualize the flow in the reactor

- motion.

The objective of the research is – Model and measure the effects of injection type and channel diameter on the two phase flow;

- - droplet formation,
 - o breakout, and
 - o coalescence

in the fiber reactor.

Present work

Design and build a prototype with viewing windows cut on the sides of the reactor.

Use light emitting particles (fluorescence) and a laser sheet, Microscope to capture visualize flow. (see figure below).,

Window cut in in the fiber reactor



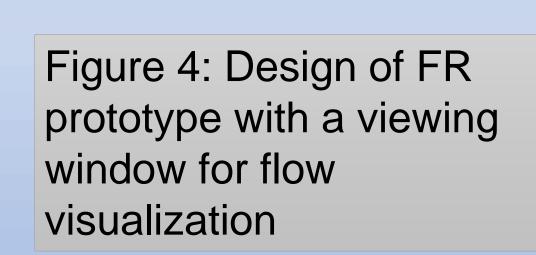
Figure 3: Mechanisms of Droplet formation and the fiber reactor

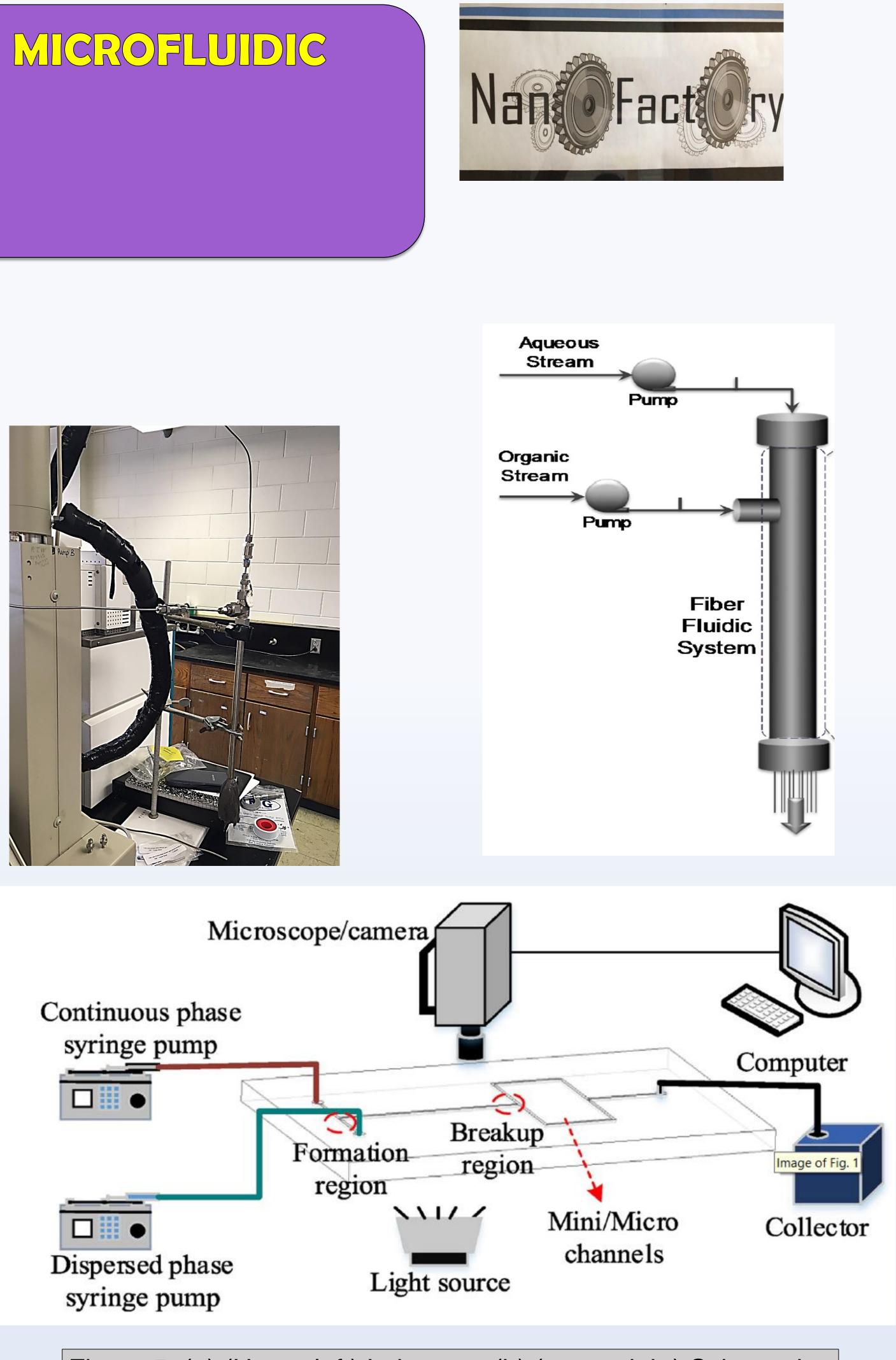


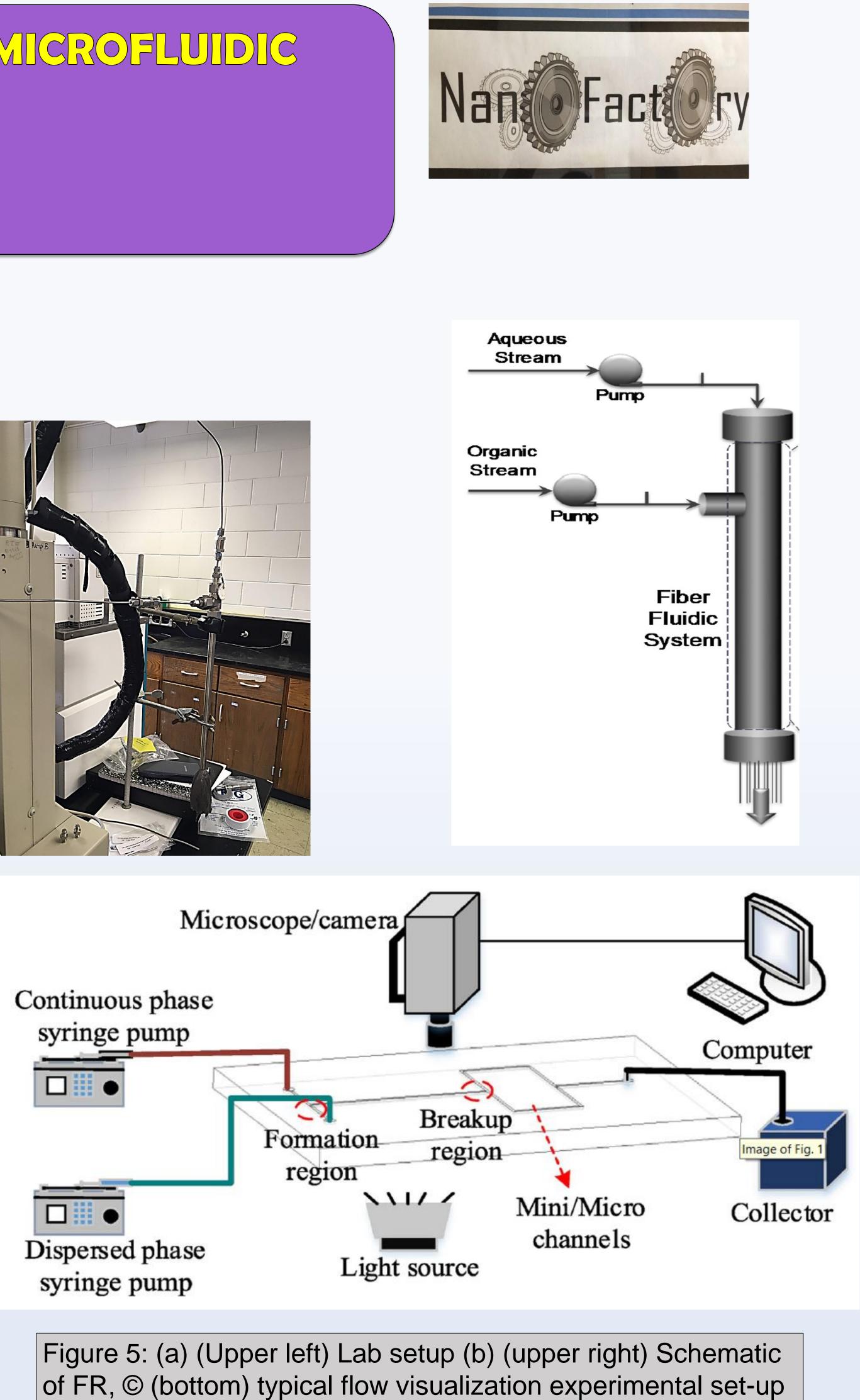
altering the fluid flow well enough so as to detect directly how the fluid flows with negligible alteration to the fluid

The approach would employ the following-

Scalar based flow visualization methods Using fluorescent or phosphorescent particles. and microscope and laser sheet.







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- 2020.

in microfluidic systems.

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